

P B M R

Process Heat Initiatives and a Focus on Hydrogen

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Nuclear Is Beyond Electricity

- Nuclear power plants today supply ~16% of global electricity
- Process heat can expand nuclear applications to other energy sectors
 - Industrial
 - Transport
 - Refineries
- Process Heat Opportunity
 - Stable process energy costs
 - Displace natural gas and other premium fuels
 - Reduce CO₂ emissions

13% 24% 24% 24% 5% 25% 13% Electricity 0 Other Industrial Transportation Refineries

World CO₂ Emissions by Sector





Shaw, Westinghouse and PBMR have teamed to produce clean, secure and economic hydrogen



B M R Heat?

Right heat delivery temperatures (up to 900°C)

- Catalyst reactions (reforming, water splitting)
- High pressure steam (oil sands and heavy oil recovery)
- Can be extended beyond 900°C once IHX technologies available

Right size and outputs (400-500MWt)

- Matches industrial plant sizes
- Matches incremental process heat demands
- Modularity enables scalability

Timely market entry

• Builds on South African Demonstration Power Plant (DPP) Project

Enhanced Safety Features

- Small nuclear footprint
- Allows proximity to customer facilities
- Easier acceptance by process industry

Clean (no CO₂)







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PBMR Process Heat Focus

• First of Fleet Power Reactor

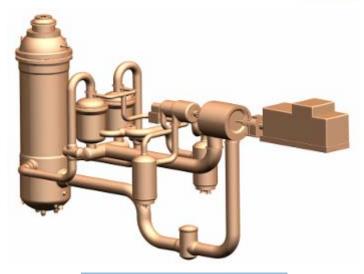
- Basic design completed; detailed design started
- International supply team in place;
- Extensive test programs underway
- Construction scheduled 2009

Process Heat Plant (PHP)

- Builds on DPP reactor design
- Produces heat up to 950°C
- Ready for operation in 2016 to 2020 time frame
- High temperature steam (400 to 500°C)
- High temperature process heat (600 to 900°C)

Next Generation Nuclear Plant (NGNP)

- Produces heat at 950°C for hydrogen production
- Completed Preconceptual Design







Process Heat Applications

Interim Goal: Process Steam (400°C to 700°C)

- Oil Sands
- Cogeneration
- Heavy oil recovery
- Desalination

Key Long-term Goal: Hydrogen (600°C to 900°C)

- Steam Methane Reforming (Hydrogen, Ammonia, Methanol)
- Water-Splitting (H₂ & O₂)
 - Bulk Hydrogen
 - Coal-to-liquids
 - Coal-to-methane

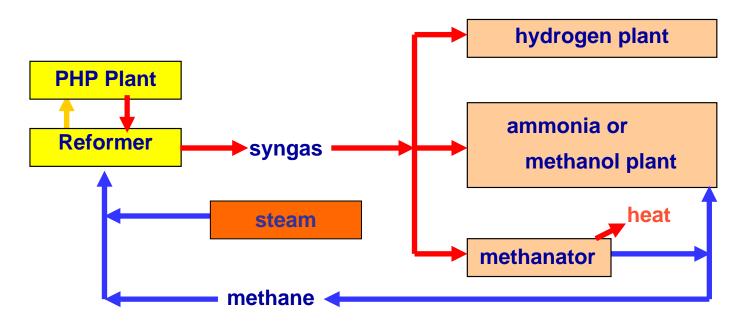


- Reduce CO₂ emissions
- Displace premium fuels
- Increase lifetime of carbon resources

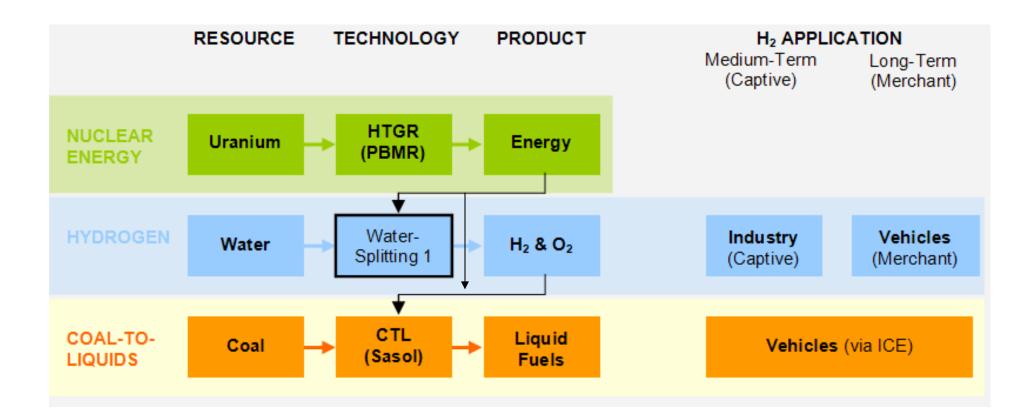
Nuclear Steam Methane P B M R Reforming – Interim Goal

Reformer Reaction

- $CH_4 + H_2O \rightarrow CO + 3H_2$ (>800°C heat required)
- PHP provides heat for reformer; displaces ~ 30% natural gas eliminates flue gas CO₂ – most expensive to capture
- Remaining heat is used for steam or power co production
- Value of syngas expected to exceed projected plant costs



Hydrogen from Water-Splitting P B M R Long Term Goal





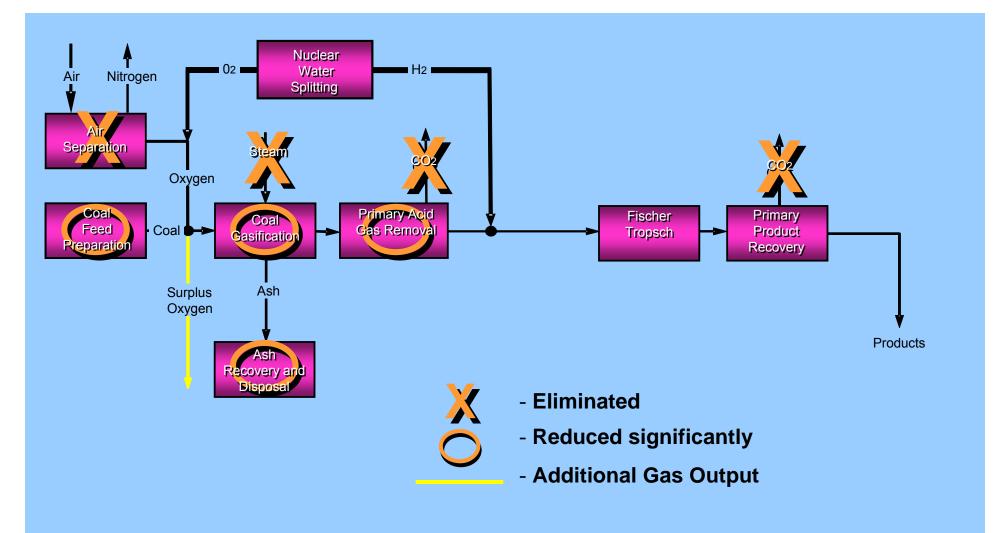
Coal-to-Liquids Concept

- Initially developed in Germany in the 1920s
- Basis for coal-to-liquid fuel production by Sasol in the Republic of South Africa
 - Provides ~30% of RSA gasoline and diesel fuel
 - Shaw/Badger is Sasol Technology partner
- New CTL projects proposed
- CTL process is a significant user of hydrogen (coal gasification)

Sasol South Africa, CTL Plant



Nuclear Water Splitting P B M R Simplifies Coal to Liquids





Value of Nuclear Water Splitting for CTL

- Displace gasification capacity, oxygen plant and related facilities dedicated to producing needed hydrogen (roughly half of syngas)
- Eliminate CO₂ production associated with converting half of coal to CO₂ just to make hydrogen
- Reduce coal consumption roughly in half

Cost of Nuclear Water Splitting

- Water splitting consumes large amounts of energy; many reactors needed for each gasifier train (producing H₂ from hydrocarbons is easier than splitting water)
- Replaces CO₂ intensive operation with capital intensive operation
- Requires development of efficient, low cost water splitting process
- Competition hinges on fossil fuel prices and CO₂ costs/credits



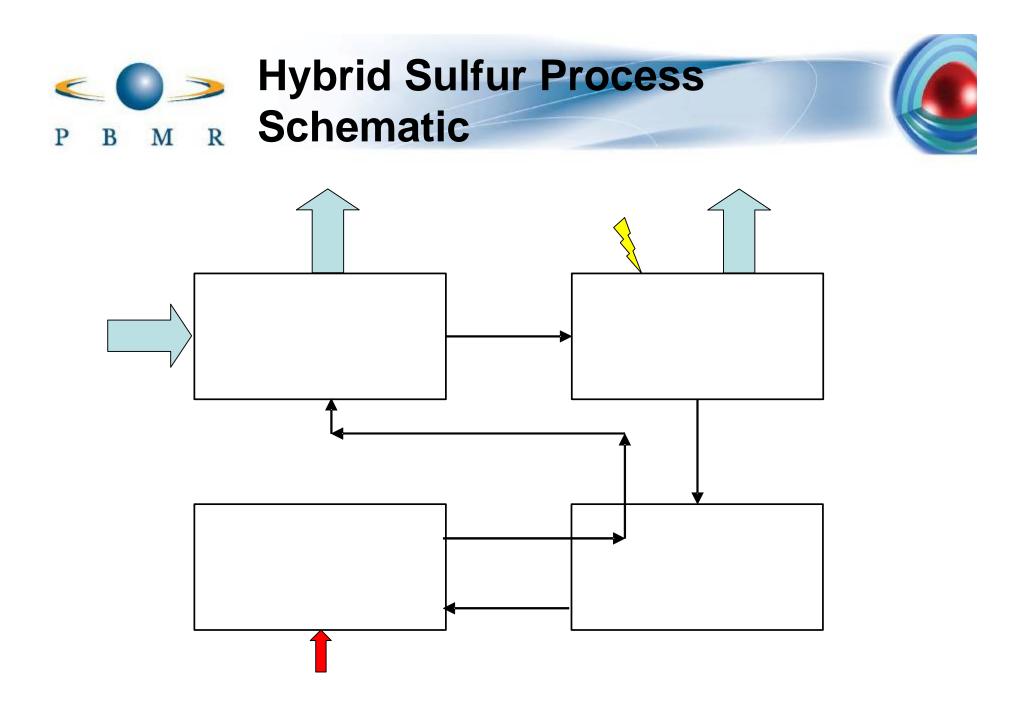
Several proposed Water-Splitting (WS) technologies evaluated

- Conventional Water Electrolysis
- High-Temperature Steam Electrolysis
- Hybrid Sulfur Process
- Sulfur Iodine Process

At present, PBMR selected the Hybrid Sulfur Process as reference cycle:

 $H_2SO_4 \rightarrow SO_2 + H_2O + \frac{1}{2}O_2$ (>800°C heat required) $2H_2O + SO_2 \rightarrow H_2 + H_2SO_4$ (electrolytic at 100°C)

- Reasonably high efficiency
- Defined flowsheet and thermodynamics
- Lowest expected costs
- However, technology development is required to commercialize Hybrid Sulfur (HyS) WS
 - PHP team part of NGNP
 - Internal PBMR and Westinghouse Electric funds committed 0



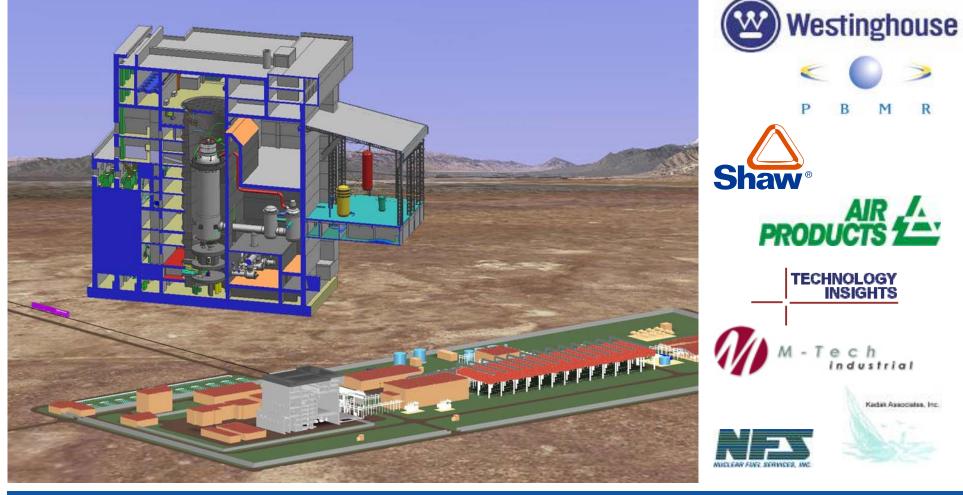


Hybrid Sulfur (HyS) History

- Work started in 1973 (Westinghouse)
- Multi-year DOE project (1976) pre-pilot bench scale demonstration by 1983
- Integrated, atmospheric pressure laboratory model constructed in 1978 (120 I/hr of H2 bench scale process operated for ~140 hours)
- Advances since 1983:
 - Equipment design and optimization (e.g., decomposition reactor)
 - Materials of construction (e.g., Nafion membranes, SiC)
- Savannah River National Laboratory (SRNL) completed pioneering work on electrolyzer
 - Successful electrolyzer test with Nafion membranes for 100 hours (May 2007)
 - Completed multicell stack electrolyzer demonstration @ 80 lph (March 2008)
 - Risk mitigation of electrolyzer technologies

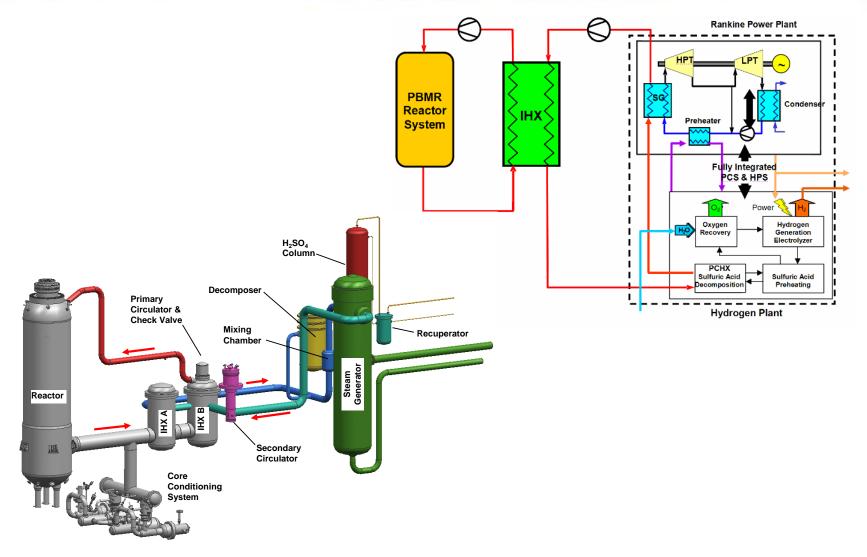


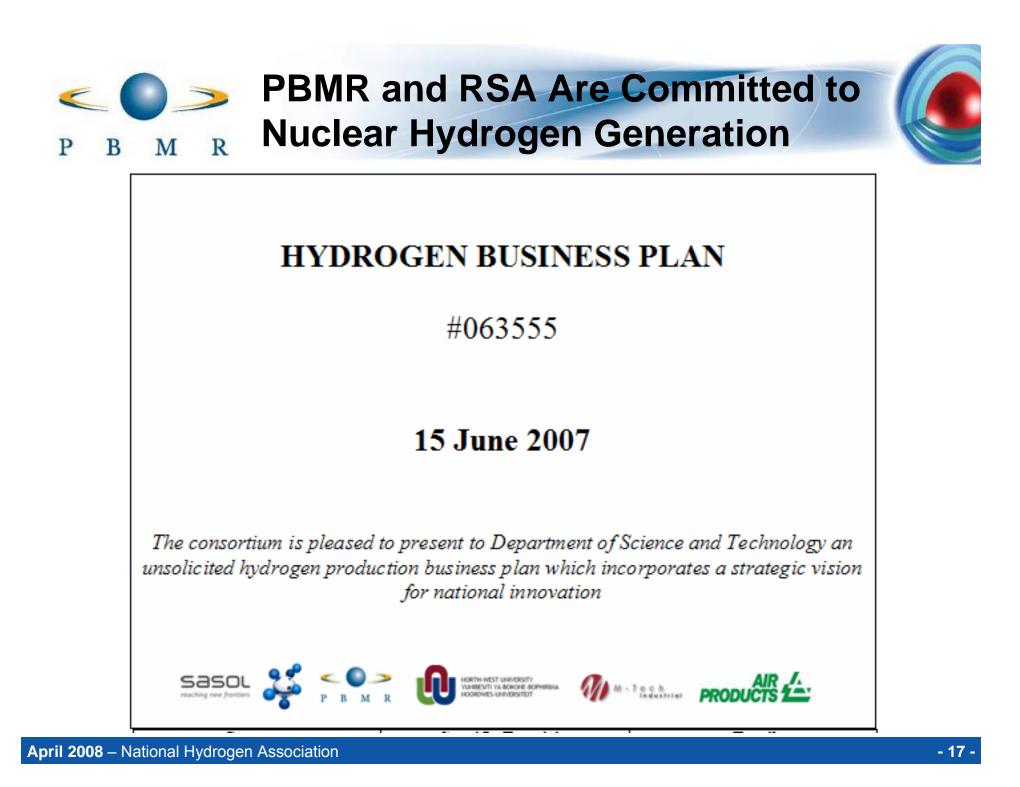
USA Department of Energy (DOE) initiative to develop a prototype plant to generate hydrogen using nuclear energy



April 2008 – National Hydrogen Association

Nuclear Water-Splitting P B M R Concept for NGNP







- PBMR provides process heat and electrical power for wide variety of applications
- Near term initiatives are in oil sands bitumen production and other steam and cogen applications
- New technology developments underway for nuclear water splitting as part of NGNP
- Innovative PBMR design, modular construction, and simplification of nuclear licensing leads to development of public support and positive government policies
- Recognition of PBMR as a CO₂ free, stable cost energy source will increase public support for PHP applications and hydrogen generation



Thank You